

1     **WHAT IS CLAIMED IS:**

- 2
- 3     1. An apparatus for converting hydrocarbon fuel into a hydrogen rich gas, comprising a
- 4         plurality of modules stacked end-to-end along a common axis, wherein each module
- 5         of the plurality of modules includes:
- 6             a shell having an interior space defining a passageway for the flow of a gas stream
- 7             from a first end of the shell to a second end of the shell opposite the first end, and
- 8             a processing core being contained within the interior space for effecting a chemical,
- 9             thermal, or physical change to the gas stream passing axially therethrough.
- 10
- 11    2. The apparatus as described in claim 1, wherein the plurality of modules are
- 12         cylindrical in shape.
- 13
- 14    3. The apparatus as described in claim 1, wherein each module of the plurality of
- 15         modules includes an annular lip at either the first end or the second end of the shell
- 16         and an annular recessed portion at the opposite end of the shell, and wherein the
- 17         annular lip of one module is receivable into the annular recess of the adjacent module.
- 18
- 19    4. The apparatus as described in claim 1, wherein at least one module of the plurality of
- 20         modules includes an annular layer of thermally insulative material disposed between
- 21         the shell and the respective processing core.
- 22
- 23    5. The apparatus as described in claim 1, wherein at least one module of the plurality of
- 24         modules includes a porous support member mounted in proximity to the first end of
- 25         the shell.
- 26
- 27    6. The apparatus as described in claim 1, wherein at least one module of the plurality of
- 28         modules includes a porous support member mounted in proximity to the second end
- 29         of the shell.
- 30

- 1 7. The apparatus as described in claim 6, wherein the porous support member is selected  
2 from the group consisting of a screen, mesh, perforated plate, and porous sintered  
3 plate.  
4
- 5 8. The apparatus as described in claim 1, wherein the plurality of modules includes a  
6 first module, wherein the processing core of the first module includes a partial  
7 oxidation catalyst.  
8
- 9 9. The apparatus as described in claim 8, wherein the first module also includes a steam  
10 reforming catalyst.  
11
- 12 10. The apparatus as described in claim 8, wherein the partial oxidation catalyst includes  
13 a metal selected from the group consisting of platinum, palladium, rhodium,  
14 ruthenium, nickel, cobalt, and any combinations thereof.  
15
- 16 11. The apparatus as described in claim 9, wherein the steam reforming catalyst includes  
17 a metal selected from the group consisting of platinum, palladium, rhodium,  
18 ruthenium, iridium, nickel, potassium, and combinations thereof.  
19
- 20 12. The apparatus as described in claim 10, wherein the metal of the partial oxidation  
21 catalyst is supported on a material selected from the group consisting of magnesia,  
22 alumina, titania, zirconia, and silica.  
23
- 24 13. The apparatus as described in claim 11, wherein the metal of the steam reforming  
25 catalyst is supported on a material selected from the group consisting of magnesia,  
26 alumina, silica, zirconia, and magnesium aluminate.  
27
- 28 14. The apparatus as described in claim 1, wherein the plurality of modules includes a  
29 second module, wherein the processing core of the second module includes a first  
30 heat exchanger for cooling the gas stream.  
31

- 1 15. The apparatus as described in claim 1, wherein the plurality of modules includes a  
2 third module, wherein the processing core of the third module includes a  
3 desulfurization agent.  
4
- 5 16. The apparatus as described in claim 14, wherein the desulfurization agent includes  
6 zinc oxide.  
7
- 8 17. The apparatus as described in claim 1, wherein the plurality of modules includes a  
9 fourth module, wherein the processing core of the fourth module includes an inert  
10 material for mixing components of the gas stream passing therethrough.  
11
- 12 18. The apparatus as described in claim 17, wherein the inert material comprises ceramic  
13 beads.  
14
- 15 19. The apparatus as described in claim 17, wherein the fourth module is designed to  
16 introduce water to the gas stream.  
17
- 18 20. The apparatus as described in claim 1, wherein the plurality of modules includes a  
19 fifth module, wherein the processing core of the fifth module includes:  
20 a water gas shift catalyst bed; and  
21 a heat exchanger positioned within the water gas shift catalyst bed for maintaining a  
22 desired shift reaction temperature range.  
23
- 24 21. The apparatus as described in claim 20, wherein the water gas shift catalyst is a low  
25 temperature water gas shift catalyst.  
26
- 27 22. The apparatus as described in claim 21 wherein the low temperature water gas shift  
28 catalyst includes a material selected from the group consisting of copper, copper  
29 oxide, zinc, platinum, rhenium, palladium, rhodium, and gold.  
30

- 1 23. The apparatus as described in claim 20, wherein the water gas shift catalyst is a high  
2 temperature water gas shift catalyst.  
3
- 4 24. The apparatus as described in claim 23, wherein the high temperature water gas shift  
5 catalyst includes a material selected from the group consisting of ferric oxide,  
6 chromic oxide, copper, iron silicide, platinum, and palladium.  
7
- 8 25. The apparatus as described in claim 1, wherein the plurality of modules includes a  
9 sixth module, wherein the processing core of the sixth module includes a second heat  
10 exchanger for cooling the gas stream.  
11
- 12 26. The apparatus as described in claim 1, wherein the plurality of modules includes a  
13 seventh module, wherein the processing core of the seventh module includes:  
14 a carbon monoxide oxidation catalyst bed; and  
15 a heat exchanger positioned within the carbon monoxide oxidation catalyst bed for  
16 maintaining a desired oxidation reaction temperature range.  
17
- 18 27. The apparatus as described in claim 26, wherein the seventh module is designed to  
19 introduce an oxygen-containing stream to the gas stream prior to contact with the  
20 carbon monoxide oxidation bed.  
21
- 22 28. The apparatus as described in claim 26, wherein the carbon monoxide oxidation  
23 catalyst bed includes a material selected from the group consisting of platinum,  
24 palladium, iron, chromium, manganese, iron oxide, chromium oxide, manganese  
25 oxide, ruthenium, palladium, gold, and any combinations thereof.  
26

1 29. An apparatus for converting hydrocarbon fuel into a hydrogen rich gas, comprising a  
2 plurality of modules stacked end-to-end along a common axis;  
3 wherein each module of the plurality of modules includes:  
4 a shell having an interior space defining a passageway for the flow of a gas stream  
5 from a first end of the shell to a second end of the shell opposite the first end,  
6 and  
7 a processing core being contained within the interior space for effecting a  
8 chemical, thermal, or physical change to the gas stream passing axially  
9 therethrough; and  
10 wherein the plurality of modules includes:  
11 a first module containing a partial oxidation catalyst bed,  
12 a second module positioned adjacent to the first module containing a first heat  
13 exchanger for cooling the gas stream,  
14 a third module positioned adjacent to the second module containing a  
15 desulfurization agent,  
16 a fourth module positioned adjacent the third module containing an inert material  
17 for mixing components of the gas stream passing therethrough,  
18 a fifth module positioned adjacent to the fourth module containing a water gas  
19 shift catalyst bed,  
20 a sixth module positioned adjacent to the fifth module containing a second heat  
21 exchanger for cooling the gas stream, and  
22 a seventh module positioned adjacent to the sixth module containing a carbon  
23 monoxide oxidation catalyst bed.

- 1 30. An apparatus for converting hydrocarbon fuel into a hydrogen rich gas, comprising a  
2 plurality of modules stacked end-to-end along a common axis;  
3 wherein each module of the plurality of modules includes:  
4 a shell having an interior space defining a passageway for the flow of a gas stream  
5 from a first end of the shell to a second end of the shell opposite the first end,  
6 and  
7 a processing core being contained within the interior space for effecting a  
8 chemical, thermal, or physical change to the gas stream passing axially  
9 therethrough; and  
10 wherein the plurality of modules includes:  
11 a first module containing a partial oxidation catalyst bed,  
12 a second module positioned adjacent to the first module containing a first heat  
13 exchanger for cooling the gas stream,  
14 a third module positioned adjacent to the second module containing a  
15 desulfurization agent,  
16 a fourth module positioned adjacent to the third module containing a water gas  
17 shift catalyst bed,  
18 a fifth module positioned adjacent to the fourth module containing a second heat  
19 exchanger for cooling the gas stream, and  
20 a sixth module positioned adjacent to the fifth module containing a carbon  
21 monoxide oxidation catalyst bed.  
22
- 23 31. A process for converting hydrocarbon fuel into a hydrogen rich gas comprising:  
24 providing a fuel processor having a plurality of modules stacked end-to-end along a  
25 common axis; and  
26 feeding the hydrocarbon fuel successively through each of the modules in an axial  
27 direction to produce the hydrogen rich gas.  
28
- 29 32. The process as described in claim 31, wherein the plurality of modules includes:  
30 a first module for the partial oxidation and steam reforming of the hydrocarbon  
31 fuel to produce a first module effluent;

- 1 a second module positioned adjacent to the first module for cooling the first
- 2 module effluent to produce a second module effluent;
- 3 a third module positioned adjacent to the second module, wherein the third
- 4 module desulfurizes the second module effluent to produce a third module
- 5 effluent;
- 6 a fourth module positioned adjacent the third module, wherein the fourth module
- 7 mixes water with the third module effluent to produce a fourth module
- 8 effluent;
- 9 a fifth module positioned adjacent to the fourth module, wherein the fifth module
- 10 reacts the water and the carbon monoxide contained in the fourth module
- 11 effluent to produce a fifth module effluent having a reduced carbon monoxide
- 12 concentration;
- 13 a sixth module positioned adjacent to the fifth module for cooling the fifth module
- 14 effluent to produce a sixth module effluent;
- 15 a seventh module positioned adjacent to the sixth module for oxidizing at least
- 16 some carbon monoxide to produce the hydrogen rich gas.
- 17
- 18 33. The process as described in claims 32, wherein the hydrocarbon fuel may be
- 19 preheated by the second module, the fifth module, the sixth module, the seventh
- 20 module, or any combination thereof.
- 21
- 22 34. The process as described in claims 32, wherein the first module operates at a
- 23 temperature ranging from about 550°C to about 900°C.
- 24
- 25 35. The process as described in claim 32, wherein the second module effluent is from
- 26 about 200°C to about 600°C.
- 27
- 28 36. The process as described in claim 32, wherein the fifth module operates at a
- 29 temperature ranging from about 150°C to about 400°C.
- 30

1 37. The process as described in claim 32, wherein the fifth module effluent is cooled to a  
2 temperature of from about 90°C to about 150°C.

3  
4 38. The process as described in claim 32, wherein the seventh module operates at a  
5 temperature of from about 90°C to about 150°C.

6  
7 The process as described in claim 32, wherein the hydrogen rich gas contains less  
8 than 50 ppm carbon monoxide.

9  
10 39. The process as described in claim 31, wherein the plurality of modules includes:

11 a first module for the partial oxidation and steam reforming of the hydrocarbon  
12 fuel to produce a first module effluent;

13 a second module positioned adjacent to the first module for cooling the first  
14 module effluent to produce a second module effluent;

15 a third module positioned adjacent to the second module, wherein the third  
16 module desulfurizes the second module effluent to produce a third module  
17 effluent;

18 a fourth module positioned adjacent to the third module, wherein the fourth  
19 module reacts water and the carbon monoxide contained in the third module  
20 effluent to produce a fourth module effluent having a reduced carbon  
21 monoxide concentration;

22 a fifth module positioned adjacent to the fourth module for cooling the fourth  
23 module effluent to produce a fifth module effluent;

24 a sixth module positioned adjacent to the fifth module for oxidizing at least some  
25 carbon monoxide to produce the hydrogen rich gas.

26  
27 40. The process as described in claims 39, wherein the hydrocarbon fuel may be  
28 preheated by the second module, the fourth module, the fifth module, the sixth  
29 module, or any combination thereof.

30



- 1 41. The process as described in claims 39, wherein the first module operates at a  
2 temperature ranging from about 550°C to about 900°C.  
3
- 4 42. The process as described in claim 39, wherein the second module effluent is from  
5 about 200°C to about 600°C.  
6
- 7 43. The process as described in claim 39, wherein the fourth module operates at a  
8 temperature ranging from about 150°C to about 400°C.  
9
- 10 44. The process as described in claim 39, wherein the fourth module effluent is cooled to  
11 a temperature of from about 90°C to about 150°C.  
12
- 13 45. The process as described in claim 39, wherein the sixth module operates at a  
14 temperature of from about 90°C to about 150°C.  
15
- 16 46. The process as described in claim 39, wherein the hydrogen rich gas contains less  
17 than 50 ppm carbon monoxide.